

1 Thermal decomposition of n-propyl and n-butyl nitrates: kinetics 2 and products

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8

9 ABSTRACT. Thermal decomposition of n-propyl (C₃H₇ONO₂, PPN) and n-butyl
10 (C₄H₉ONO₂, BTN) nitrates have been studied in a low pressure flow reactor combined with a
11 quadrupole mass spectrometer. The rate constants of the nitrates decomposition were
12 measured as a function of pressure (0.95 -12.8 Torr of helium) and temperature in the range
13 473 – 659 K using two different approaches: from kinetics of nitrate loss and those of the
14 formation of the reaction products. The fit of the observed falloff curves with two parameter
15 expression $k = \frac{k_0 k_\infty [M]}{k_0 [M] + k_\infty} \times 0.6^{(1 + (\log(\frac{k_0 [M]}{k_\infty}))^2)^{-1}}$ provided the following low and high
16 pressure limits for the rate constants of the nitrates decomposition: $k_0(\text{PPN}) = 0.68 \times 10^{-4} \exp(-$
17 $15002/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$, $k_\infty(\text{PPN}) = 7.34 \times 10^{15} \exp(-19676/T) \text{ s}^{-1}$, $k_0(\text{BTN}) = 2.80 \times 10^{-4}$
18 $\exp(-15382/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ and $k_\infty(\text{BTN}) = 7.49 \times 10^{15} \exp(-19602/T) \text{ s}^{-1}$, which allow to
19 reproduce (via above expression and with 20% uncertainty) all the experimental data obtained
20 for the rate constants of PPN and BTN decomposition in the temperature and pressure range
21 of the study. It was observed that the initial step of the thermal decomposition of the nitrates
22 is O–NO₂ bond cleavage leading to formation of NO₂ and alkoxy radical, which rapidly
23 decomposes or isomerizes to form C₂H₅ and formaldehyde and C₃H₇, CH₂O and hydroxybutyl
24 radical as final products of PPN and BTN decomposition, respectively. In addition, the kinetic
25 data were used to determine the O–NO₂ bond dissociation energy of 38.0 ± 1.2 and 37.8 ± 1.0
26 kcal mol⁻¹ in PPN and BTN, respectively.
27

28 **Keywords:** propyl nitrate, butyl nitrate, thermal decomposition, rate constant, falloff curve,
29 alkoxy radical.

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34 **1. Introduction**

35 Organic nitrates are important species in atmospheric and combustion chemistry. In the
36 atmosphere, they are formed in a minor addition channel of the reaction of peroxy radicals
37 with NO and also in the NO₃-initiated oxidation of unsaturated organic compounds [1].
38 Organic nitrates are considered as stable species with atmospheric lifetimes of several days or
39 weeks (depending on their photolysis rate and reactivity toward OH radicals [2]), and play a
40 key role in the distribution of reactive nitrogen by undergoing long-range transport in the free
41 troposphere. In combustion processes, nitrates, used as fuel additives, are known to promote
42 the ignition of diesel fuel. Production of chain-initiating radicals and, possibly, the heat
43 released during nitrate decomposition in the pre-ignition phase are thought to decrease the
44 ignition-delay time [3-5].

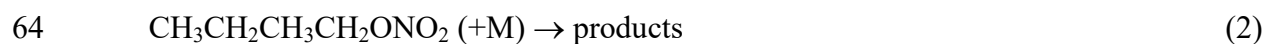
45 Thermal decomposition of acyclic nitrates is supposed to proceed through a radical
46 mechanism with initial dissociation of the O–NO₂ bond leading to formation of NO₂ and
47 alkoxy radical (RO):



49 The alkoxy radicals can undergo a number of competing reaction pathways, including
50 unimolecular decomposition, which usually occurs through C–C bond fission to produce a
51 carbonyl compound, and a unimolecular isomerization, which generates a hydroxy-substituted
52 alkyl radical [6].

53 Although thermal decomposition of nitrates has been studied previously for several times
54 [7-15], available quantitative information on the rate constants and products of these reactions
55 is very scarce. To our knowledge, no experimental data are available for thermal
56 decomposition of n-butyl nitrate and those for n-propyl nitrate pyrolysis were reported in two
57 studies only [13,16]. In our recent paper [17], we have reported the results of the experimental
58 study of the kinetics and products of the thermal decomposition of isopropyl nitrate. In the

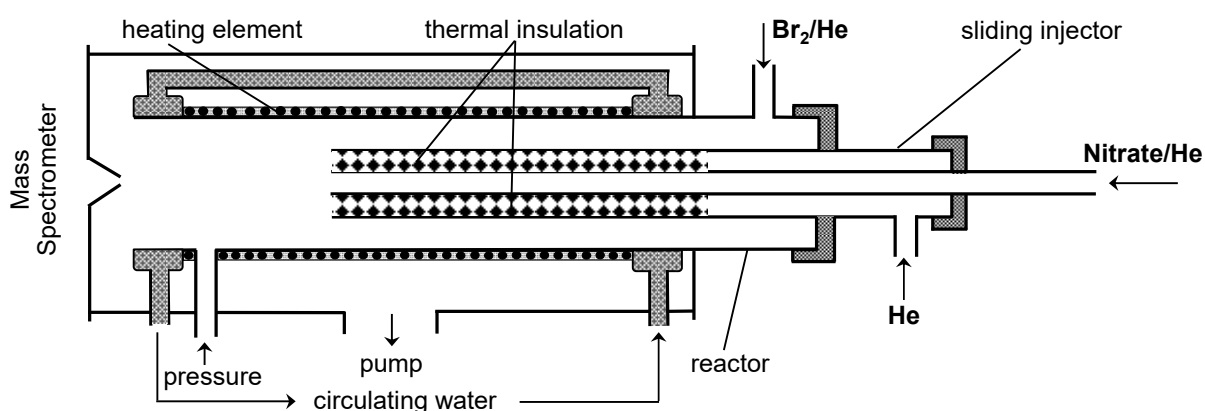
59 present work, we applied a similar experimental approach to study thermal decomposition of
60 n-propyl (PPN) and n-butyl (BTN) nitrates, including the measurements of the rate constants
61 as a function of pressure and temperature and identification and quantification of the reaction
62 products:



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66 2. Materials and methods

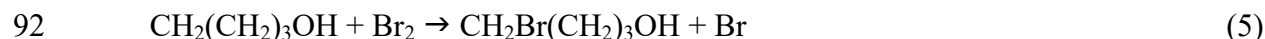
67 Thermal decomposition of the nitrates was studied at a total pressure of helium between 0.95
68 and 12.8 Torr and in the temperature range (473 - 659) K. Experiments were carried out in a
69 flow reactor using a modulated molecular beam electron impact ionization (with ion source
70 operating at 25-30 eV) mass spectrometer as the detection method [17,18]. The flow reactor
71 (Fig. 1) consisted of a Quartz tube (45 cm length and 2.5 cm i.d.) with an electrical heater and
72 water-cooled extremities [18]. Temperature in the reactor was measured with a *K*-type
73 thermocouple positioned in the middle of the reactor in contact with its outer surface.
74 Temperature gradient along the flow tube measured with a thermocouple inserted in the
75 reactor through the movable injector was less than 1% [18].



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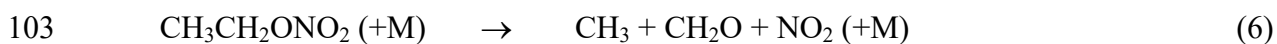
77 **Fig. 1** Diagram of the flow reactor.

78 The nitrates were introduced into the flow reactor through the movable injector (that
79 allowed to vary their residence time in the reactor) from a 10L flasks containing nitrate-He
80 mixture or (when high concentrations of the nitrates were needed) by passing helium through
81 a thermostated glass bubbler containing liquid nitrate. The inner tube of the injector, through
82 which nitrates were supplied, was thermally insulated in order to minimize their possible
83 decomposition prior introduction into the main reactor (Fig. 1). Both nitrates was detected by
84 mass spectrometry at their fragment peak at $m/z = 76$ ($\text{CH}_2\text{ONO}_2^+$), which is much more
85 intensive than the parent ones (at $m/z = 105$ and 119 , for PPN and BTN, respectively). C_2H_5 ,
86 C_3H_7 and hydroxybutyl ($\text{C}^*\text{H}_2\text{CH}_2\text{CH}_2\text{CH}_2\text{OH}$) radicals were detected as bromoethane, 1-
87 bromopropane and 4-bromo-1-butanol at $m/z = 108/110$ ($\text{C}_2\text{H}_5\text{Br}^+$), $122/124$ ($\text{C}_3\text{H}_7\text{Br}^+$) and
88 fragment peak $134/136$ ($\text{CH}_2\text{Br}(\text{CH}_2)_2\text{CH}^+$), respectively, after being scavenged by an excess
89 of Br_2 ($[\text{Br}_2] \sim 5 \times 10^{13}$ molecule cm^{-3}) via reactions [19]:



93 All other species were detected at their parent peaks: $m/z = 30$ (formaldehyde, CH_2O^+), 160
94 (Br_2^+), 46 (NO_2^+).

95 The absolute calibration of mass spectrometer for formaldehyde was realized by injecting
96 known amounts (0.2 – 0.8 μL) of the 36.5 % wt solution of CH_2O in water inside the flow tube,
97 and recording the parent mass peak intensity of CH_2O at $m/z = 30$. The integrated area of the
98 mass spectrometric signals corresponding to known total number of CH_2O molecules injected
99 into the reactor allowed the determination of the calibration factor. Similar procedure was
100 applied for the measurements of the absolute concentrations of 4-bromo-1-butanol. Another
101 alternative method used for absolute calibrations of CH_2O consisted in thermal decomposition
102 of ethyl nitrate (at $T \geq 600\text{K}$) in the presence of Br_2 in the reactor:



104 (products of this reaction were studied in an unpublished work from our group).
105 Experimentally, total consumption of the nitrate and appearance of the decomposition
106 products, NO_2 and CH_2O , was observed and absolute concentrations of the species could be
107 determined in accordance with: $[\text{CH}_2\text{O}] = [\text{NO}_2] = [\text{C}_2\text{H}_5\text{ONO}_2]_0$. The results of this
108 calibration method were in good agreement (within 10-15%) with that by injection of CH_2O
109 and measurements of $[\text{NO}_2]$ from their calibrated mixtures. The absolute calibration of mass
110 spectrometer for other stable species (Br_2 , $\text{C}_2\text{H}_5\text{Br}$, $\text{C}_3\text{H}_7\text{Br}$, $\text{C}_2\text{H}_5\text{ONO}_2$, $\text{C}_3\text{H}_7\text{ONO}_2$,
111 $\text{C}_4\text{H}_7\text{ONO}_2$) was realized through calculation of their absolute concentrations in the reactor
112 from their flow rates obtained from the measurements of the pressure drop of their mixtures in
113 He stored in calibrated volume flasks.

114 Ethyl and n-propyl nitrates were synthesized in the laboratory via slow mixing of the
115 corresponding alcohol with $\text{H}_2\text{SO}_4:\text{HNO}_3$ (1:1) mixture at temperature $< 5^\circ\text{C}$ [20,21]. The
116 synthesized nitrate was degassed before use. The purities and origin of other gases used were
117 as follows: He $>99.9995\%$ (Alphagaz); Br_2 $>99.99\%$ (Aldrich); NO_2 $> 99\%$ (Alphagaz); 36.5
118 % wt solution of formaldehyde in water (Sigma-Aldrich); n-butyl nitrate $> 99\%$ (Chemos);
119 bromoethane ($\geq 99\%$, Sigma-Aldrich); 1-bromopropane ($\geq 99\%$, Sigma-Aldrich); 4-bromo-1-
120 butanol ($\geq 85\%$, Aldrich).

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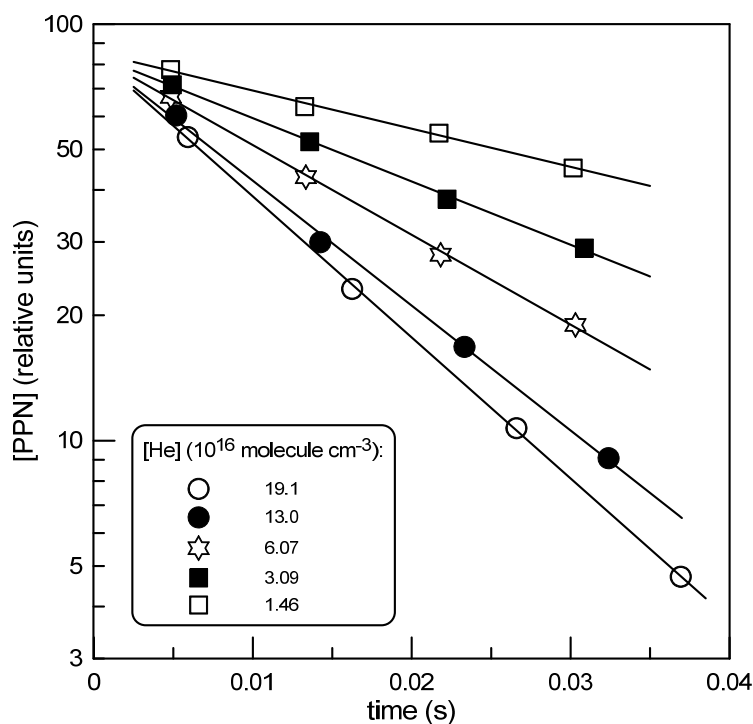
122 **3. Results and discussion**

123 We employed two different methods for the measurements of the rate of nitrate
124 decomposition [17]. The first one, used at higher temperatures ($T = 563 - 659$ K), consisted in
125 a direct monitoring of the kinetics of nitrate loss. In the second approach, used at lower
126 temperatures ($T = 473 - 577$ K), where consumption of nitrate was too low to be measured

127 accurately, the rate constant was determined from the kinetics of the reaction product
128 formation.

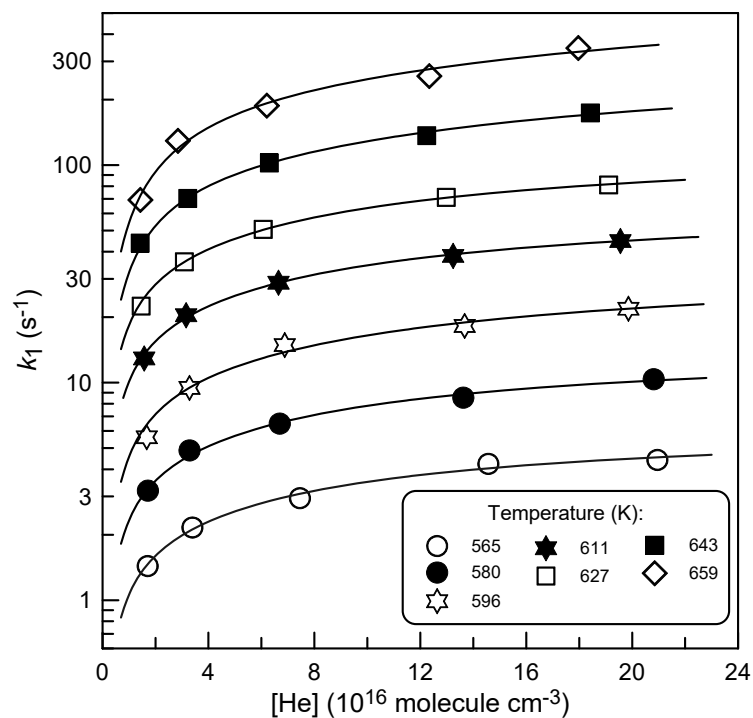
129 3.1. Kinetics of *n*-propyl and *n*-butyl nitrate decomposition

130 In this series of experiments the rate constant of reactions (1) and (2) was determined from the
131 kinetics of nitrate loss due to its decomposition. It was observed that at a given total pressure
132 consumption of nitrate follows first order kinetics: $d[\text{Nitrate}]/dt = -k \times [\text{Nitrate}]$. Example of
133 the exponential decays of *n*-propyl nitrate observed at different pressures in the reactor at $T =$
134 627 K is shown in Fig. 2.



135
136 **Fig. 2** Example of kinetics of *n*-propyl nitrate decomposition at different pressures of He in the reactor: $T =$
137 627 K.

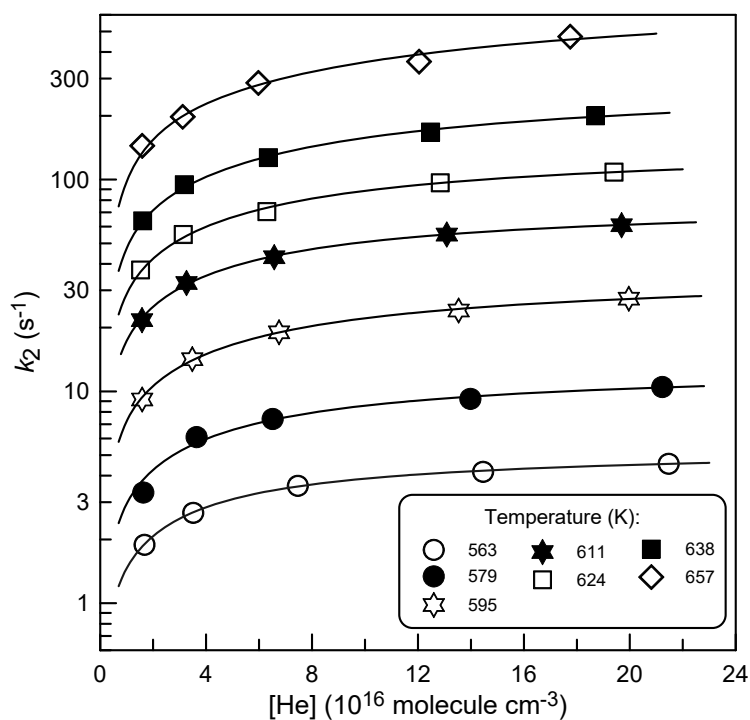
138 The values of k_1 and k_2 (in s^{-1}) determined from the loss kinetics of PPN and BTN (like those
139 shown in Fig. 2) at different temperatures in the reactor are plotted in Fig. 3 and 4 as a
140 function of total pressure. The uncertainty on the measurements of the rate constants was
141 estimated to be nearly 10%, including statistical error (within a few percent) and those on the
142 measurements of the flows (5%), pressure (2%) and temperature (1%).



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Fig. 3 Rate of n-propyl nitrate decomposition measured at different temperatures from kinetics of the nitrate loss as a function of total pressure of He. Uncertainty on k_1 (nearly 10%) corresponds to the size of symbols. Continuous lines represent the best fit to the experimental data according to equations (I) and (II) with $F_c = 0.6$ and two varied parameters, k_0 and k_∞ .



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Fig. 4 Rate of n-butyl nitrate decomposition measured at different temperatures from kinetics of BTN loss as a function of total pressure of He. Uncertainty on k_2 (nearly 10%) corresponds to the size of symbols. Continuous lines represent the best fit to the experimental data according to equations (I) and (II) with $F_c = 0.6$ and two varied parameters, k_0 and k_∞ .

154 One can note that in the pressure range of the present study, decomposition of nitrates
 155 proceeds in the “falloff regime” (Fig. 3 and 4). Generally the dependence of the rate constant
 156 on pressure in falloff regime is described using the Lindemann-Hinshelwood reaction scheme:



159 with addition of a broadening factor, F , to the Lindemann-Hinshelwood expressions [22,23],
 160 leading to

$$k = \frac{k_0 k_\infty [M]}{k_0 [M] + k_\infty} F = k_0 [M] \left(\frac{1}{1 + k_0 [M] / k_\infty} \right) F \quad (I)$$

161 where $k_0 = k_7$ and $k_\infty = k_7 k_8 / k_{-7}$ are low and high pressure limits of the rate constant,
 162 respectively, and the broadening factor F is determined as:

$$\log F \cong \frac{\log F_c}{1 + \left(\frac{\log(k_0 [M] / k_\infty)}{N} \right)^2} \quad (II)$$

163 with $N = 0.75-1.27 \log F_c$ [22,23]. So the falloff curve is characterized by three parameters,
 164 k_0 , k_∞ and F_c (called “center broadening factor”), all being reaction- and temperature-
 165 dependent. In practice, it is impossible to fit a limited part of falloff curve, usually determined
 166 in experiments, with three variable parameters. In the present study, as in our previous work
 167 on decomposition of isopropyl nitrate [17], in order to describe the dependence of the rate
 168 constant on pressure we adopted simplified approach used in JPL evaluation of kinetic data
 169 [24]: the experimental falloff curve was fitted accordingly to equations (I) and (II) with fixed
 170 and independent of temperature $F_c = 0.6$ and $N = 1$ and two varied parameters, k_0 and k_∞ .
 171 Obviously, k_0 and k_∞ determined in this way depend on the choice of F_c -value, nevertheless
 172 this procedure allows to describe the experimental data with the three clearly specified
 173 parameters.

174 Continuous lines in Fig. 3 and 4 represent the fit to the experimental data according to
 175 equations (I) and (II) with $F_c = 0.6$, providing the values of k_0 and k_∞ for decomposition of
 176 PPN and BTN at different temperatures, which are summarized in Tables I and II,
 177 respectively.

178
 179 **Table I**
 180 Thermal decomposition of n-propyl nitrate: summary of the measurements of k_0 and k_∞ .

T (K)	k_0 (10^{-15} cm ³ molecule ⁻¹ s ⁻¹) ^a	k_∞ (s ⁻¹) ^a	Method ^b
473	0.00101	0.00635	C ₂ H ₅ kinetics
488	0.00237	0.0264	C ₂ H ₅ kinetics
503	0.00811	0.0753	C ₂ H ₅ kinetics
518	0.0163	0.231	C ₂ H ₅ kinetics
533	0.0492	0.647	C ₂ H ₅ kinetics
549	0.105	1.66	C ₂ H ₅ kinetics
564	0.198	4.66	C ₂ H ₅ kinetics
565	0.196	7.45	PPN kinetics
577	0.360	8.83	C ₂ H ₅ kinetics
580	0.419	17.2	PPN kinetics
596	0.747	41.5	PPN kinetics
611	1.77	78.8	PPN kinetics
627	3.19	147	PPN kinetics
643	4.74	389	PPN kinetics
659	8.08	853	PPN kinetics

181 ^a estimated uncertainty factor of 1.5,

182 ^b see text.

183

184 **Table II**
 185 Thermal decomposition of n-butyl nitrate: summary of the measurements of k_0 and k_∞ .

T (K)	k_0 (10^{-15} cm ³ molecule ⁻¹ s ⁻¹) ^a	k_∞ (s ⁻¹) ^a	Method ^b
484	0.00470	0.019	products kinetics
499	0.0120	0.071	products kinetics
514	0.0259	0.205	products kinetics
531	0.090	0.612	products kinetics
545	0.183	1.65	products kinetics
561	0.411	4.8	products kinetics

563	0.394	6.06	BTN kinetics
579	0.676	15	BTN kinetics
595	1.51	41.7	BTN kinetics
611	3.92	89.6	BTN kinetics
624	6.00	167	BTN kinetics
638	8.65	341	BTN kinetics
657	15.7	926	BTN kinetics

186 ^a estimated uncertainty factor of 1.5,

187 ^b see text.

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189 The measurements of k_1 and k_2 were carried out with initial concentration of nitrate $\leq 10^{12}$
190 molecule cm^{-3} . In a special series of experiments, we have verified for the possible influence
191 of the initial concentration of PPN (at $P = 8.3$ Torr and $T = 602$ K) and BTN (at $P = 8.2$ Torr
192 and $T = 611$ K) on the measured values of k_1 and k_2 . The rates of PPN and BNT
193 decomposition were found to be independent (within 5%, for PPN see Fig. S1 in
194 Supplementary data) of their initial concentrations varied in the range (0.09 – 2.40) and (0.15
195 – 1.90) $\times 10^{12}$ molecule cm^{-3} , respectively.

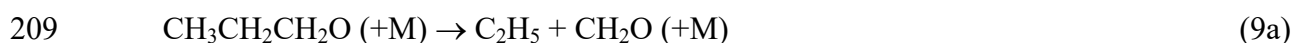
196 Decomposition of the nitrates on the wall of the flow reactor could potentially impact the
197 measured rates of their loss. Adams & Bawn [8] in their study of ethyl nitrate decomposition
198 under static conditions reported that a 7.4 times increase in surface of a Pyrex reaction vessel
199 had no influence on the reaction rate at $T = 456$ K, indicating on a limited impact of the wall
200 processes. This finding allows to expect a negligible (compared with homogeneous process)
201 heterogeneous loss of PPN and BTN in our fast flow quartz reactor, although in the present
202 study the decomposition of the nitrates on the wall of the reactor was not tested.

203 **3.2. Reaction products**

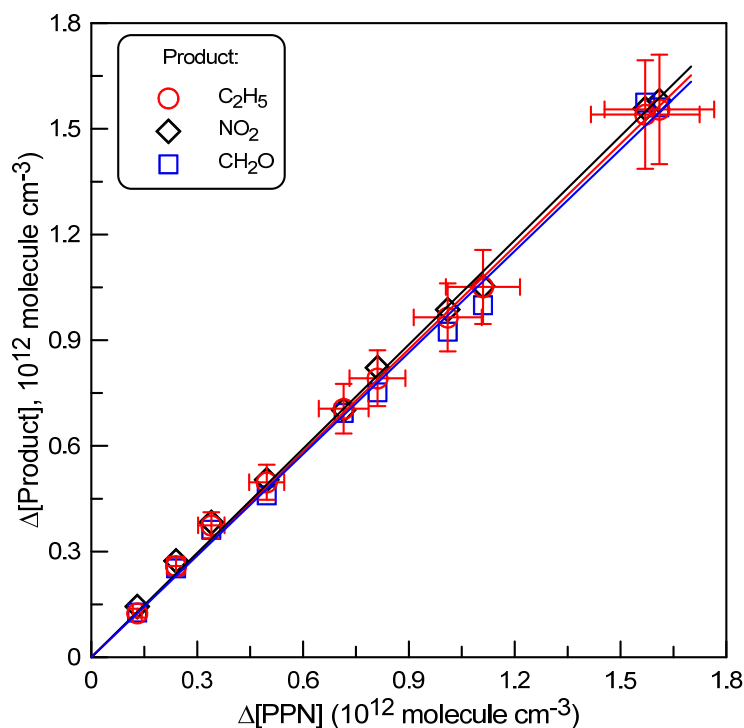
204 Thermal decomposition of n-propyl nitrate is expected to proceed through initial dissociation
205 of the O–NO₂ bond leading to formation of NO₂ and propoxy radical:



207 The n-propoxy radical, CH₃CH₂CH₂O, can undergo unimolecular decomposition through the
208 following two competitive reaction pathways [6,25]:



211 Based on the rate constants calculated for reactions (9a) and (9b) [6,25], one could expect that
212 under experimental conditions of the present study (i) C₂H₅ forming channel (9a) is the
213 dominant one ($k_{9b}/k_{9a} < 0.002$) and (ii) decomposition of the n-propoxy radical is very rapid
214 on the timescale of our experiments ($k_{9a} > 10^4 \text{ s}^{-1}$). Indeed, we have observed the formation of
215 NO₂, C₂H₅ and formaldehyde (CH₂O) upon decomposition of n-propyl nitrate in the flow
216 reactor. There is an important contribution of n-propyl nitrate to the MS signals of NO₂ and
217 CH₂O due to its fragmentation in the ion source of the mass spectrometer. That is why the
218 quantitative measurements of the yields of the three reaction products were carried out under
219 conditions where almost complete decomposition of PPN was observed. Experiments
220 consisted in the monitoring of the concentrations of the products formed upon total
221 decomposition of PPN in the reactor in the presence of relatively high concentration of Br₂
222 ($[\text{Br}_2] \sim 5 \times 10^{13} \text{ molecule cm}^{-3}$) in order to transform C₂H₅ radicals into C₂H₅Br. Initial
223 concentration of PPN was varied in the range $(0.13 - 1.61) \times 10^{12} \text{ molecule cm}^{-3}$. The results of
224 these experiments are shown in Fig. 5.



225

226 **Fig. 5** Concentration of the products formed upon decomposition of n-propyl nitrate as a function of
 227 consumed concentration of PPN: P = 8.5 Torr, T = 630 K. Error bars correspond to 10% uncertainty on the
 228 measurements of the PPN and product concentrations.
 229

230 The slopes of the straight lines in Fig. 5 provide the yields of the corresponding species:

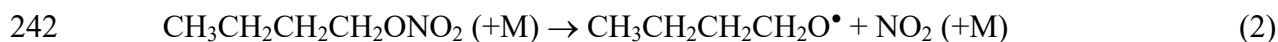
231
$$\Delta[\text{NO}_2]/\Delta[\text{PPN}] = 0.99 \pm 0.15,$$

232
$$\Delta[\text{CH}_2\text{O}]/\Delta[\text{PPN}] = 0.96 \pm 0.15,$$

233
$$\Delta[\text{C}_2\text{H}_5]/\Delta[\text{PPN}] = 0.97 \pm 0.15,$$

234 The estimated nearly 15% uncertainty on the measurements arises mainly from the combined
 235 errors on the measurements of the absolute concentrations of n-propyl nitrate and reaction
 236 products. These results confirm that the O–NO₂ bond cleavage is the initial step of PPN
 237 decomposition and C–C bond fission leading to formation of C₂H₅ and formaldehyde is the
 238 predominant decomposition pathway of the n-propoxy radical under experimental conditions
 239 of the study.

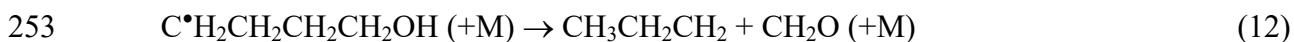
240 In the case of reaction (2), the situation is somewhat more complex. The 1-butoxy radical
 241 (CH₃CH₂CH₂CH₂O•) formed upon decomposition of n-butyl nitrate,



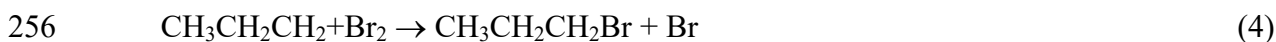
243 in addition to its decomposition, can also isomerize to four hydroxybutyl radicals:
 244 $\text{CH}_3\text{CH}_2\text{CH}_2\text{C}^\bullet\text{HOH}$, $\text{CH}_3\text{CH}_2\text{C}^\bullet\text{HCH}_2\text{OH}$, $\text{CH}_3\text{C}^\bullet\text{HCH}_2\text{CH}_2\text{OH}$ and $\text{C}^\bullet\text{H}_2\text{CH}_2\text{CH}_2\text{CH}_2\text{OH}$.
 245 The available experimental and theoretical data [26] show that under the experimental
 246 conditions of the present study (temperature and pressure range) the dominant processes of 1-
 247 butoxy radical transformation are its decomposition to propyl radical and formaldehyde and
 248 isomerization to $\text{C}^\bullet\text{H}_2\text{CH}_2\text{CH}_2\text{CH}_2\text{OH}$ hydroxybutyl radical:



251 The most favorable channels for the $\text{C}^\bullet\text{H}_2\text{CH}_2\text{CH}_2\text{CH}_2\text{OH}$ radical are its back isomerization
 252 to 1-butoxy radical (reaction (-11)) and decomposition to C_3H_7 and CH_2O [26]:



254 In the presence of bromine in our flow reactor, the propyl and hydroxybutyl radicals are
 255 expected [19] to react with Br_2 to form 1-bromopropane and 4-bromo-1-butanol, respectively:

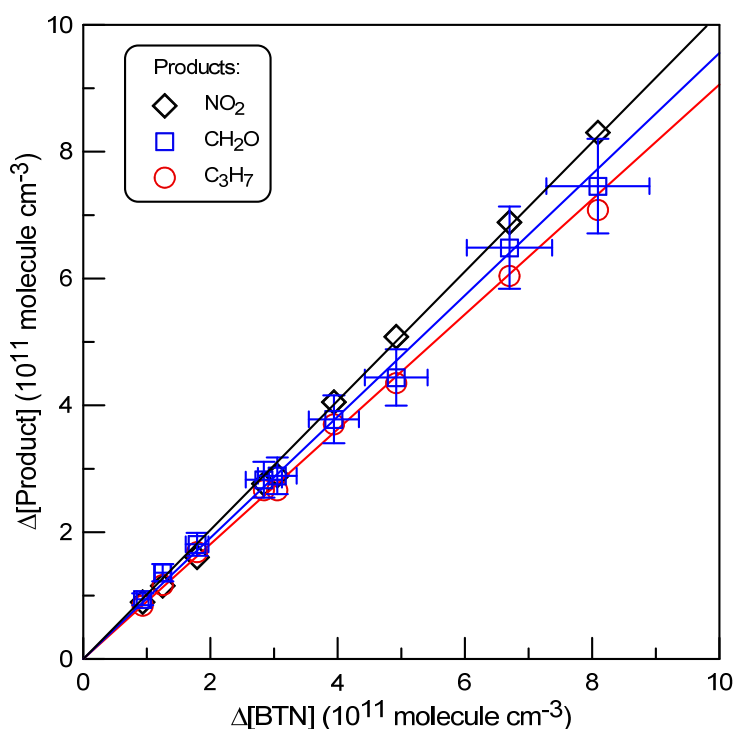


258 Indeed, in our experiments on thermal decomposition of n-butyl nitrate in the presence of Br_2
 259 we have observed the production of both 1-bromopropane ($\text{C}_3\text{H}_7\text{Br}^+$ at $m/z = 122/124$) and 4-
 260 bromo-1-butanol (at its fragment peaks at $m/z = 134/136$). It was observed that the
 261 distribution of these two brominated reaction products depended on the concentration of Br_2
 262 in the reactor: increase of Br_2 concentration resulted in increase of 4-bromo-1-butanol and
 263 decrease of 1-bromopropane yield. This experimental observation reflects the concurrent
 264 consumption of $\text{C}^\bullet\text{H}_2\text{CH}_2\text{CH}_2\text{CH}_2\text{OH}$ radical in reactions (-11), (12) and (5). In addition,
 265 relative concentrations of 1-bromopropane and 4-bromo-1-butanol were found to depend also

266 on pressure and temperature because reactions (10) – (12) have different pressure and
267 temperature dependences.

268 The results of the measurements of the yields of the products formed upon decomposition
269 of BTN in the presence of Br_2 ($\sim 5 \times 10^{13}$ molecule cm^{-3}) in the reactor at $T = 640$ K are shown
270 in Fig. 6.

271



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273

274 **Fig. 6** Concentration of the products formed upon decomposition of n-butyl nitrate as a function of
275 consumed concentration of BTN: $P = 4$ Torr, $T = 640$ K. Error bars correspond to characteristic 10%
276 uncertainty on the measurements of the concentrations of BTN and reaction products.

277

278 The slopes of the straight lines in Fig. 6 provide the yields of the corresponding species:

279
$$\Delta[\text{NO}_2]/\Delta[\text{PPN}] = 1.02 \pm 0.15,$$

280
$$\Delta[\text{CH}_2\text{O}]/\Delta[\text{PPN}] = 0.96 \pm 0.15,$$

281
$$\Delta[\text{C}_3\text{H}_7]/\Delta[\text{PPN}] = 0.91 \pm 0.15,$$

282 The yield of 4-bromo-1-butanol, which was found to have a trend to decrease with increase of
283 temperature, was measured to be $< 5\%$ in these experiments.

284 As noted above, the products of the thermal decomposition of propyl and butyl nitrates
285 were investigated in the presence of Br₂ in the reactor leading to formation of Br atoms in
286 reactions (3-5). The concentration of Br atoms in the reactor is expected to be similar to those
287 of the reaction products, i.e. $\leq 1.6 \times 10^{12}$ molecule cm⁻³. The possible side reactions of Br
288 atoms with brominated alkanes C₂H₅Br and C₃H₇Br are relatively slow and have a negligible
289 impact on the concentrations of these species under experimental conditions of the
290 measurements. The rate constant of the reaction of Br with C₃H₇Br was reported in only one
291 study:



$$293 \quad k_{13} = 2.09 \times 10^{-12} \exp(-3580/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1} \quad (T = 374-483\text{K}) [27],$$

294 providing $k_{13} \approx 7.8 \times 10^{-15}$ cm³ molecule⁻¹ s⁻¹ at highest temperature of the measurements T =
295 640K, i.e. $k'_{13} = k_{13} \times [\text{Br}] < 0.01 \text{ s}^{-1}$. The reaction of Br atoms with C₂H₅Br is expected to be
296 even slower. Another reaction which potentially could have an impact on the observed
297 products of reactions (1) and (2) is the reaction of Br atoms with CH₂O:



$$299 \quad k_{14} = 7.7 \times 10^{-12} \exp(-580/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1} \quad (T = 220-300\text{K}) [28].$$

300 No data for the reaction rate constant are available at high temperatures. Extrapolation of the
301 existing measurements to $T = 630 \text{ K}$ gives the value of the rate constant of nearly 3×10^{-12}
302 cm³ molecule⁻¹ s⁻¹. Even with maximal concentration of $[\text{Br}] = 1.6 \times 10^{12}$ molecule cm⁻³ the
303 consumption of CH₂O in reaction with Br at $T = 630 \text{ K}$ would be less than 15% (reaction time
304 $\approx 30 \text{ ms}$). The observed linear dependence of the concentrations of the reaction products on
305 the consumed concentration of the nitrate (Fig. 5 and 6) can be considered as an additional
306 experimental evidence of the negligible role of the secondary reactions of Br atoms.

307

308

309 3.3. Measurements of k_1 and k_2 from kinetics of product formation

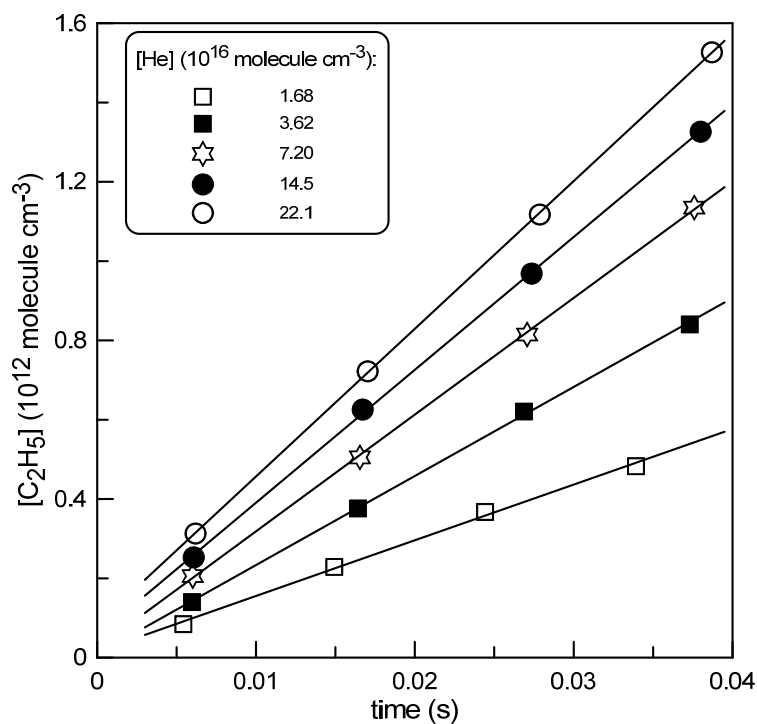
310 In this series of experiments, carried out at lower temperatures, the rate constants of reactions
311 (1) and (2) were determined from the kinetics of product formation under conditions where
312 consumption of the nitrates was negligible and the rate constants could not be determined
313 from their decays. For reaction (1), CH_3CH_2 radical was chosen among three products of PPN
314 decomposition because the mass spectra of NO_2 and formaldehyde were highly perturbed by
315 contribution of the fragment peaks of n-propyl nitrate which was present in the reactor at
316 relatively high concentrations. Br_2 was added in the reactor in order to convert C_2H_5 radicals
317 to $\text{C}_2\text{H}_5\text{Br}$, which was monitored by mass spectrometry. As one could expect, linear increase
318 of C_2H_5 concentration with reaction time was observed upon decomposition of n-propyl
319 nitrate (Fig. S2 in Supplementary data) in line with expression:

$$320 \quad \frac{d[\text{C}_2\text{H}_5]}{dt} = k_1 \times [\text{PPN}] \quad (\text{III})$$

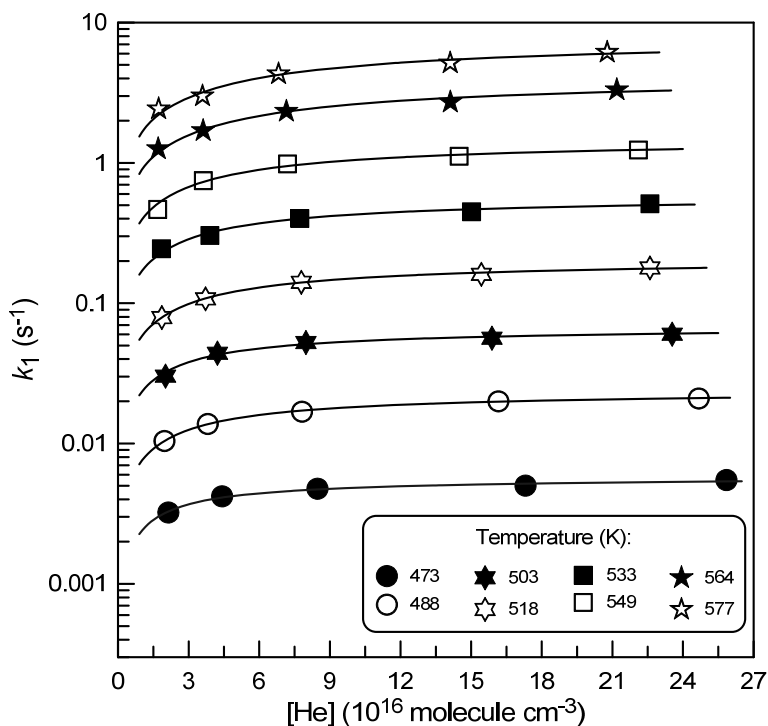
321 and under conditions where variation of PPN concentration with time was insignificant (<
322 10%). The slopes of the straight lines in Fig. S2 provide the rate of C_2H_5 production,
323 $d[\text{C}_2\text{H}_5]/dt$ (in molecule $\text{cm}^{-3}\text{s}^{-1}$), which is presented in Fig. S3 (Supplementary data) as a
324 function of initial concentration of PPN. The observed linear, in accordance with equation
325 (III), dependence of $d[\text{C}_2\text{H}_5]/dt$ on [PPN] indicates negligible contribution of possible
326 secondary reactions which could lead to C_2H_5 production or consumption.

327 Example of kinetics of C_2H_5 formation measured at different pressures in the reactor is
328 shown in Fig. 7. All the experimental data obtained for k_1 ($k_1 = 1/[\text{PPN}] \times d[\text{C}_2\text{H}_5]/dt$) from the
329 kinetics of C_2H_5 production at different pressures and temperatures are shown in Fig. 8.
330 Procedure, similar to that used above in the case of PPN loss kinetics, was employed to
331 extract low and high pressure limits of k_1 : continuous lines in Fig. 8 represent the best fit to
332 the experimental data according to equations (I) and (II) with $F_c = 0.6$ and two varied

333 parameters, k_0 and k_∞ . The results obtained for k_0 and k_∞ in this series of experiments are
 334 presented in Table I.



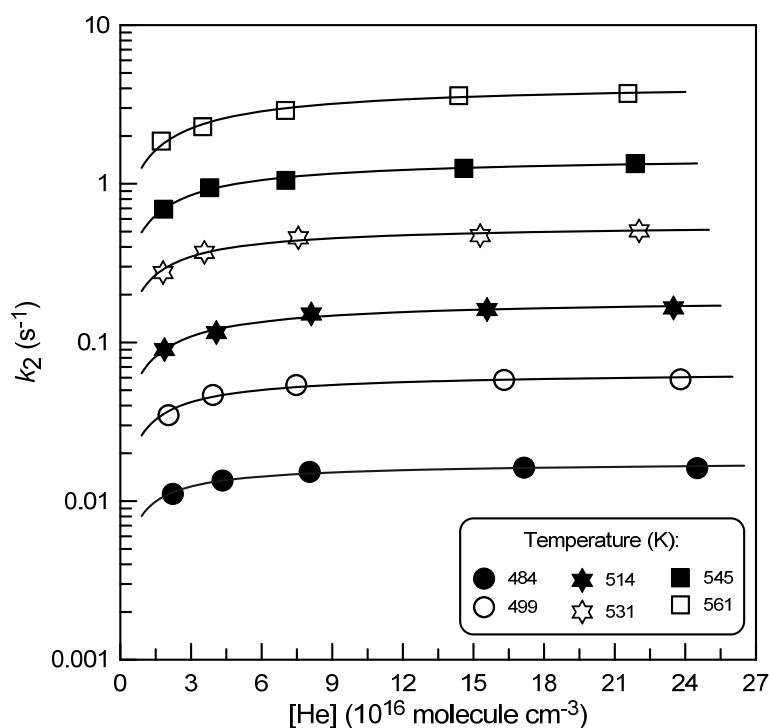
335
 336 **Fig. 7** Kinetics of C_2H_5 production upon PPN decomposition measured at different pressures in the reactor:
 337 $T = 549\text{ K}$, $[PPN] = 3.0 \times 10^{13}\text{ molecule cm}^{-3}$.
 338



339
 340 **Fig. 8** Rate constant of C_2H_5 production upon PPN decomposition as a function of total pressure of He at
 341 different temperatures in the reactor. Height of the symbols corresponds to nearly 15% uncertainty on k_1 .
 342

343

344 Similar approach was employed for the measurements of k_2 . However, in this case, given
345 the complex dependence of the yields of the two main brominated products, 1-bromopropane
346 and 4-bromo-1-butanol, on pressure, temperature and concentration of Br_2 , in the
347 measurements of k_2 from the kinetics of product formation we used the sum of the
348 concentrations of these species, disregarding the distribution between them. The experimental
349 data obtained for k_2 ($k_2 = 1/[\text{BTN}] \times d([\text{C}_3\text{H}_7] + [\text{C}^\bullet\text{H}_2(\text{CH}_2)_3\text{OH}])/dt$) at different pressures and
350 temperatures are shown in Fig. 9.



351

352 **Fig. 9** Rate constant of reaction (2) measured from the kinetics of 1-bromopropane and 4-bromo-1-butanol
353 production upon BTN decomposition in the presence of Br_2 as a function of total pressure of He at different
354 temperatures in the reactor. Height of the symbols corresponds to nearly 15% uncertainty on k_2 .

355

356 Low and high pressure limits of k_2 , resulting from the best fit to the experimental data in Fig.
357 9 according to equations (I) and (II) with $F_c = 0.6$, are presented in Table 2.

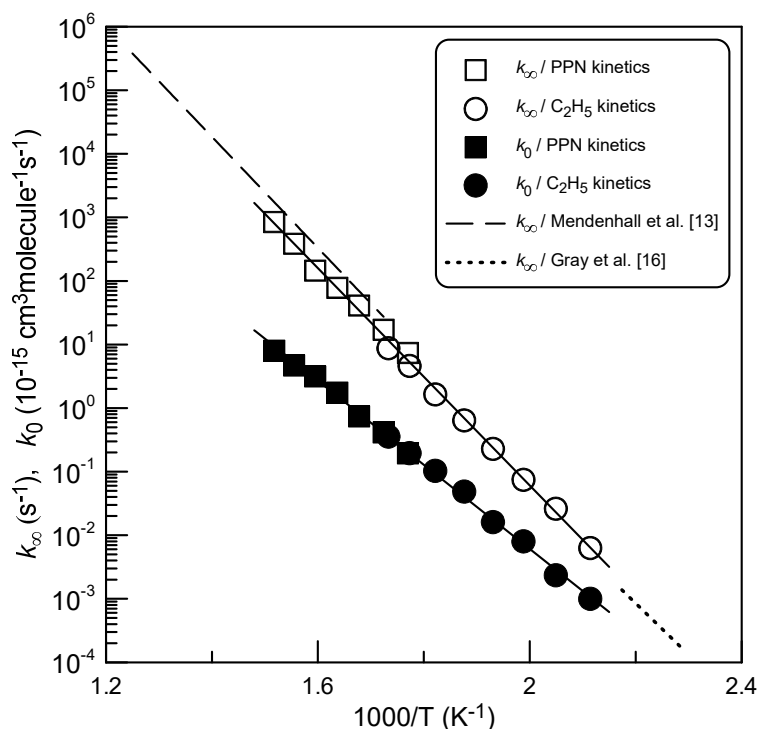
358 Concerning the uncertainty on k_0 and k_∞ derived from the fit of the falloff curves (with
359 fixed value of $F_c = 0.6$) in Fig. 3, 4, 8 and 9, it depends on the temperature of the

360 measurements and has a different trend for low and high pressure limits of k_1 and k_2 . For
 361 example, it is obvious that at lower temperatures (Fig. 8 and 9), the simulated falloff curve is
 362 more sensible to the value of k_∞ and less to the value of k_0 , because k_1 and k_2 are relatively
 363 close to their high pressure limits. To keep things simple, we place a conservative (nearly
 364 maximum) estimated uncertainty of a factor of 1.5 on all the derived values of k_0 and k_∞ .

365

366 3.4. Temperature dependence of k_1 and k_2

367 Temperature dependences of the low and high pressure limits of k_1 and k_2 are shown in Fig.
 368 10 and 11, respectively. One can note good agreement between the results obtained from the
 369 kinetics of the nitrate loss and those of the products formation. The combination of two
 370 approaches allowed the determination of the rate constants over a range of nearly 5 orders of
 371 magnitude.

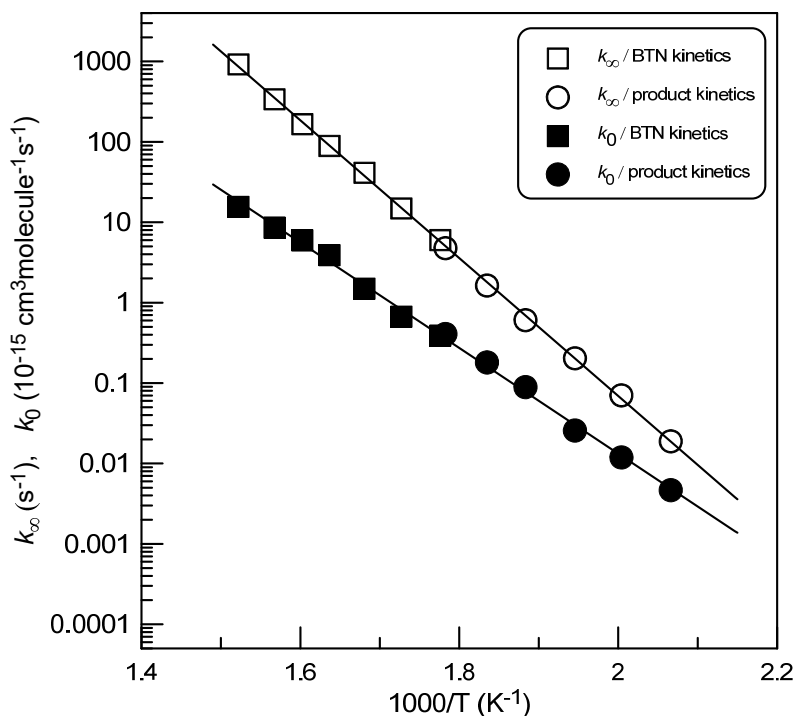


372

373 **Fig. 10** Thermal decomposition of n-propyl nitrate: temperature dependence of the high and low pressure
 374 limits of k_1 .

375

376



377

378 **Fig. 11** Thermal decomposition of n-butyl nitrate: temperature dependence of the high and low pressure
 379 limits of k_2 .

380

381 Unweighted exponential fit to the experimental data in Fig. 10 and 11 provides the following

382 Arrhenius expressions: k_∞ (PPN) = $7.46 \times 10^{15} \exp(-19675/T) \text{ s}^{-1}$ and k_0 (PPN) = 1.02×10^{-4}

383 $\exp(-15225/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$, k_∞ (BTN) = $9.54 \times 10^{15} \exp(-19732/T) \text{ s}^{-1}$ and k_0 (BTN) =

384 $1.78 \times 10^{-4} \exp(-15115/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$.

385 In the above analysis, the temperature dependence of the low and high pressure limits of

386 the rate constant was determined from the individual values of these parameters determined at

387 each temperature. We applied also another approach which consisted of a global fitting of all

388 the experimental data simultaneously accordingly to equations (I) and (II) with fixed and

389 independent of temperature $F_c = 0.6$ and $N = 1$ and variable pre-exponential factors and

390 activation energies in Arrhenius expressions for k_∞ and k_0 . The expressions for k_∞ and k_0

391 obtained within this approach did not differ significantly from those presented above and are

392 recommended from the present study:

393 k_∞ (PPN) = $7.34 \times 10^{15} \exp(-19676/T) \text{ s}^{-1}$,

394 $k_0(\text{PPN}) = 0.68 \times 10^{-4} \exp(-15002/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$,

395 $k_\infty(\text{BTN}) = 7.49 \times 10^{15} \exp(-19602/T) \text{ s}^{-1}$

396 $k_0(\text{BTN}) = 2.80 \times 10^{-4} \exp(-15382/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$

397 It should be emphasized again that the reported values of k_∞ and k_0 depend on the choice of
398 the F_c -value used in the fitting of falloff curves and should be considered just as parameters
399 allowing to represent the experimentally measured temperature and pressure dependence of k_1
400 and k_2 as:

401
$$k = \frac{k_0 k_\infty [M]}{k_0 [M] + k_\infty} \times 0.6^{(1 + (\log(\frac{k_0 [M]}{k_\infty}))^2)^{-1}}$$

402 This expression in combination with k_∞ and k_0 given above reproduces all the
403 temperature and pressure dependence data obtained for k_1 and k_2 in the present study
404 with accuracy within 20 and 15%, respectively, and thus can be recommended for
405 calculation of k_1 and k_2 in the temperature ranges 473 – 659 K and 484 – 657 K,
406 respectively, and He pressures between 1 and 12.8 Torr with conservative uncertainty
407 of 20%.

408 As noted above the absolute values of k_∞ and k_0 determined in the present study depend
409 on the F_c -value used in the calculations. We conducted an analysis of the sensitivity of k_∞ and
410 k_0 to the choice of the F_c -value. For that the global fit of all the experimental data (shown in
411 Tables S1 and S2 of Supplementary data) to expressions (I) and (II) was performed using
412 different values of F_c . The results obtained for low and high pressure limits of k_1 and k_2 are
413 shown in Tables S3 and S4 (Supplementary data), respectively. The last columns in Tables S3
414 and S4 show the mean (for 75 and 65 experimental data points, respectively) of the ratios of
415 calculated (using expressions (I) and (II) with different F_c -factors and corresponding set of
416 Arrhenius parameters) and experimental values of k_1 and k_2 , respectively. One can note that
417 the experimental rate constant data can be described adequately and with a similar precision

418 with any value of F_c between 0.3 and 0.8. On the other hand, the activation energies, E_∞ and
419 E_0 , are rather insensitive to the choice of F_c -factors, and seem to be well defined by the
420 measured values of k_1 and k_2 . Considering the data presented in Tables S3 and S4, we place
421 less than 7% uncertainty on the activation energies in Arrhenius expressions for k_∞ and k_0
422 recommended above (for $F_c = 0.6$ and $N = 1$): E_∞ (PPN) = (19676 ± 600), E_0 (PPN) = (15002
423 ± 1000), E_∞ (BTN) = (19602 ± 500) and E_0 (BTN) = (15382 ± 500) K.

424 We failed to find in the literature any quantitative experimental data on thermal
425 decomposition of n-butyl nitrate. Concerning n-propyl nitrate, to our knowledge, the
426 quantitative data on its decomposition were reported only in two previous publications
427 [13,16]. Mendenhall et al. [13], applying RRKM theory to the experimental data from their
428 Very-Low-Pressure study of PPN pyrolysis at $T = (580 - 800)$ K, derived the high pressure
429 rate expression of k_1 , k_∞ (PPN) = $3.16 \times 10^{16} \exp(-20118/T) \text{ s}^{-1}$. Gray et al. [16], referring to
430 Ph.D thesis of L. Phillips (London, 1949), reported k_∞ (PPN) = $5.01 \times 10^{14} \exp(-18600/T) \text{ s}^{-1}$
431 in rather narrow temperature range $T = (438 - 460)$ K. The values of k_∞ (PPN) calculated with
432 these expressions are shown in Fig. 10 and seem to be in satisfactory agreement with those
433 from the present study.

434 The activation energies obtained in the present work for k_∞ , E_∞ (PPN) = 39.1 ± 1.2 and
435 E_∞ (BTN) = $38.9 \pm 1.0 \text{ kcal mol}^{-1}$, allows the determination of the O–NO₂ bond dissociation
436 energy (BDE) in n-propyl and n-butyl nitrates as $\text{BDE} = E_\infty - RT_{\text{av}}$, where T_{av} is the average
437 temperature of the T -range used in experiments:

$$438 \quad \text{BDE} (\text{C}_3\text{H}_7\text{O}-\text{NO}_2) = 38.0 \pm 1.2 \text{ kcal mol}^{-1}$$

$$439 \quad \text{BDE} (\text{C}_4\text{H}_9\text{O}-\text{NO}_2) = 37.8 \pm 1.0 \text{ kcal mol}^{-1}$$

440 These values are in good agreement with the O–NO₂ bond dissociation energy of 38.3
441 and 38.2 kcal mol^{-1} in n-propyl and n-butyl nitrates, respectively, calculated by
442 Khrapkovskii et al. [29] using density-functional B3LYP method. Zeng et al. [30]

443 using different DFT methods calculated O–NO₂ bond dissociation energy in n-propyl
444 nitrate in the range (34.1-42.2) kcal mol⁻¹, which overlaps the experimental value from
445 this work. It seems that the extensive experimental data from the present study could
446 serve as a basis for further theoretical developments.

447

448 **4. Conclusions**

449 In this work, kinetics and products of the thermal decomposition of n-propyl and n-
450 butyl nitrates were investigated. The rate constants of the reactions were measured as a
451 function of temperature, T = (473-659) K, in the pressure range (0.95-12.8) Torr of
452 helium. NO₂ was directly observed as a primary product of the decomposition of both
453 nitrates and its yield (nearly unity) was measured. The co-product of NO₂ in the
454 decomposition of n-propyl nitrate, propoxy radical C₃H₇O, was found to rapidly
455 decompose on the timescale of our experiments leading to practically exclusive
456 production of C₂H₅ radical and formaldehyde in the temperature range of the study. In
457 contrast, for the butoxy radical (CH₃(CH₂)₃O), formed in a first stage of n-butyl nitrate
458 decomposition, both decomposition to propyl radical and formaldehyde and
459 isomerization to hydroxybutyl radical, C[•]H₂(CH₂)₃OH, was observed. The O-NO₂
460 bond dissociation energy in n-propyl and n-butyl nitrates were determined as (38.0 ±
461 1.2) and (37.8 ± 1.0) kcal mol⁻¹, respectively.

462

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467

468 **Appendix A. Supplementary data**

469 Supplementary data associated with this article can be found, in the online version, at ...

470

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512

513 **Figure captions**

514

515 **Fig. 1** Diagram of the flow reactor.

516 **Fig. 2** Example of kinetics of n-propyl nitrate decomposition at different pressures of He in
517 the reactor: T = 627 K.

518 **Fig. 3** Rate of n-propyl nitrate decomposition measured at different temperatures from
519 kinetics of the nitrate loss as a function of total pressure of He. Uncertainty on k_1 (nearly
520 10%) corresponds to the size of symbols. Continuous lines represent the best fit to the
521 experimental data according to equations (I) and (II) with $F_c = 0.6$ and two varied parameters,
522 k_0 and k_∞ .

523 **Fig. 4** Rate of n-butyl nitrate decomposition measured at different temperatures from kinetics
524 of BTN loss as a function of total pressure of He. Uncertainty on k_2 (nearly 10%) corresponds
525 to the size of symbols. Continuous lines represent the best fit to the experimental data
526 according to equations (I) and (II) with $F_c = 0.6$ and two varied parameters, k_0 and k_∞ .

527 **Fig. 5** Concentration of the products formed upon decomposition of n-propyl nitrate as a
528 function of consumed concentration of PPN: P = 8.5 Torr, T = 630 K. Error bars correspond
529 to 10% uncertainty on the measurements of the PPN and product concentrations.

530 **Fig. 6** Concentration of the products formed upon decomposition of n-butyl nitrate as a
531 function of consumed concentration of BTN: P = 4 Torr, T = 640 K. Error bars correspond to
532 characteristic 10% uncertainty on the measurements of the concentrations of BTN and
533 reaction products.

534 **Fig. 7** Kinetics of C_2H_5 production upon PPN decomposition measured at different pressures
535 in the reactor: T = 549 K, $[PPN] = 3.0 \times 10^{13}$ molecule cm^{-3} .

536 **Fig. 8** Rate constant of C_2H_5 production upon PPN decomposition as a function of total
537 pressure of He at different temperatures in the reactor. Height of the symbols corresponds to
538 nearly 15% uncertainty on k_1 .

539 **Fig. 9** Rate constant of reaction (2) measured from the kinetics of 1-bromopropane and 4-
540 bromo-1-butanol production upon BTN decomposition in the presence of Br_2 as a function of
541 total pressure of He at different temperatures in the reactor. Height of the symbols
542 corresponds to nearly 15% uncertainty on k_2 .

543 **Fig. 10** Thermal decomposition of n-propyl nitrate: temperature dependence of the high and
544 low pressure limits of k_1 .

545 **Fig. 11** Thermal decomposition of n-butyl nitrate: temperature dependence of the high and
546 low pressure limits of k_2 .

547